

**BR&E ProMax<sup>®</sup> 3.x (Build 3.2.10286.0) Release Notes**  
**13 October 2010**  
**Bryan Research & Engineering, Inc.**

Welcome to ProMax 3.2 (build 3.2.10286.0). This upgrade is a maintenance upgrade to earlier ProMax 3.x releases and contains several new features and stability improvements. If you need assistance or would like to report a problem in ProMax, please contact our technical support group at [support@bre.com](mailto:support@bre.com). You may also consult our frequently asked questions list at <http://www.bre.com/support/promax-faq.aspx>. In addition to common usage questions, this list contains solutions to common problems related to program installation. Finally, we would encourage you to seek our assistance in questions related to program applicability. ProMax is a robust, accurate simulator that can be used in many processes.

These release notes describe the major changes that have occurred between the ProMax 3.x release and the ProMax 2.0 release. Refer to the release notes from previous versions of ProMax to determine the significant changes made within a specific release and the changes made relative to the predecessors of ProMax, PROSIM<sup>®</sup> and TSWEET<sup>®</sup>. These can also be requested by email from our support group at [support@bre.com](mailto:support@bre.com).

ProMax utilizes Microsoft Visio<sup>®</sup> 2002, Microsoft Visio 2003, Microsoft Visio 2007, or Microsoft Visio 2010 as its drawing package. All flowsheets are drawn using Visio. You must have a legal copy of either Microsoft Visio 2002, 2003, 2007, or 2010 (x86) Premium, Professional, or Standard to use ProMax through its GUI. **This particular version of ProMax is not compatible with other releases of Visio, including any future releases.** The version of Visio installed on your computer can be found by using the Help->About menu item in Visio. Microsoft offers a 60 day trial version of Visio on its website at <http://office.microsoft.com/visio>. Additionally, depending on the version, Visio requires a patch from Microsoft to use successfully with ProMax. See Obtaining the Required Visio Patch section below for more details.

The following table lists the operating system compatibility with ProMax 3.x. Special attention should be paid to the notes concerning your respective operating system. Upgrading the operating system is strongly recommended for any system that is not in the mainstream support phase of Microsoft as BR&E does not perform routine testing of ProMax on these platforms and full compatibility is suspect. For all systems, a minimum of 512 MB of RAM is required, with more usually required depending on operating system, application load, and other software needs.

<b>Operating System</b>	<b>Edition</b>	<b>Notes</b>
Windows 2000	Professional or Server	Requires SP4 and IE6 SP1. Also requires MDAC 2.8 SP1 manual installation prior to ProMax installation. MDAC and the MDAC Component Checker utility (used to determine current installed version) are available from <a href="http://www.microsoft.com/downloads">http://www.microsoft.com/downloads</a> . Immediate upgrade recommended as BR&E will

		not support this platform in the next major release due to support termination by Microsoft. Microsoft ended the extended support phase for Windows 2000 on 13 July 2010.
Windows XP	All x86	Requires SP2 with SP3 recommended. Recommend upgrading SP2 systems with hotfixes <a href="http://support.microsoft.com/kb/921337">http://support.microsoft.com/kb/921337</a> and <a href="http://support.microsoft.com/kb/943232">http://support.microsoft.com/kb/943232</a> prior to installing ProMax to avoid potential problems during install. Users of SP3 systems that fail during MSXML configuration in the SQL install should see <a href="http://www.bre.com/support/promax-faq.aspx">http://www.bre.com/support/promax-faq.aspx</a> for a solution. Microsoft support for SP2 ended 13 July 2010.
Windows XP	Professional x64	SP2 required
Windows Server 2003	x86 or x64	SP2/R2 required
Windows Vista	All x86 and x64	RTM/SP1/SP2 Microsoft support for RTM ended 10 April 2010.
Windows Server 2008	All x86 and x64	SP1/SP2/R2
Windows Server 2008 R2	x86 unavailable	RTM
Windows 7	All x86 and x64	RTM

When ProMax is loaded by Visio, Visio will issue a warning concerning the presence of macros. This warning is provided by Microsoft Office applications to warn you of the possible presence of viruses that may be present within the macros. Microsoft has created a strategy where the macros are digitally signed by their author so you are assured of their integrity. Digital signatures require a trusted third party to verify the authenticity of the signature and its data. Not all macros are signed. The author of unsigned macros is unknown and usually should be considered suspect. All BR&E documents pertaining to Visio or other Microsoft Office applications are digitally signed. This digital signature can be verified by inspecting the certificate displayed in the warning message. You must allow or trust all BR&E signed macros to execute or you will prevent ProMax from functioning properly. You should add BR&E to your trusted list of macros to ensure proper execution of ProMax.

### **Obtaining the Required Visio Patch or Service Pack in Visio 2002 & 2003**

During ProMax development in mid 2003, BR&E discovered a problem in Microsoft Visio that can cause corruption in files saved in ProMax or Visio due to loss of digital certificate signatures. While this problem was discovered during the initial beta test period for Visio 2003, we were unable to determine the exact cause of the problem with Microsoft at that time and consequently a solution was not obtainable. Early in 2004, we discovered the fundamental cause of the problem and were able to work with Microsoft to develop a Visio patch to solve this issue.

The digital certificate problem is present in both Visio 2002 and Visio 2003. Unfortunately, it may be more severe in Visio 2002 because the problem is present without warning to the user.

With the release of Microsoft Office 2003 products, Microsoft set the default macro security level in documents to high. This causes any document with a missing digital certificate to fail on load. However, in Visio 2002, the default macro security level is medium which does not cause failure on load. Files saved with Visio 2002 will likely fail if the user upgrades to Visio 2003 if the digital signature has been silently lost unless the security level is changed.

You can determine if the minimum patch level is met by inspecting the full build available from the Help->About menu item in Visio. For Visio 2003, the build number must be 11.4301.6360 or greater. For Visio 2002, the build number must be 10.0.6002 or greater.

For Visio 2003 users, the patch has been rolled into Service Pack 2 (and Service Pack 3) for Visio 2003 which may be downloaded from the Microsoft Office website at <http://office.microsoft.com/en-us/officeupdate/default.aspx>. This update is normally applied through the automatic updating process in Microsoft Windows and does not require manual installation. However, for Visio 2002 users, the method to obtain the fix is through a Visio patch or hotfix. As of this writing the patch has not been rolled into a Visio 2002 Service Pack. Due to copyright restrictions, the patch must be obtained directly from Microsoft. You can obtain the patch for Visio 2002 (10.0.6002) by following the instructions in the Microsoft Knowledge Base article 890668 available at <http://support.microsoft.com/?id=890668>. Note that you must apply Visio 2002 Service Pack 2 before installing this patch. Due to the severity of this problem and the potential for data loss, ProMax will issue a warning each time you start the application if this patch is not installed. There should be no cost involved with obtaining the patch. Please contact our customer support if you have questions or problems with the above requirement.

## **Warnings and Warranty**

The user assumes full responsibility for the results and application obtained from the use of ProMax. No implied warranty of merchantability, no implied warranty of fitness for any purpose, and no implied warranty arising by usage of trade, course of dealing, or course of performance is given by BR&E or shall arise from ProMax.

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ProMax is protected by copyright law and international treaties. Unauthorized reproduction, distribution, reverse engineering, or use of this program, or any portion of it, may result in severe civil and criminal penalties and will be prosecuted to the maximum extent possible under law.

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## **Installation of ProMax 3.x**

ProMax uses Windows Installer Service 3.1 (WIS) technology for installation. The installer supports standard as well as administrative installs through a file or application server. In this

release, a security device is not required to perform the installation. However, you must have a valid BR&E security device present to run ProMax. To install ProMax on a workstation, you must either be an administrator, or you must have elevated installation privileges set through either an IntelliMirror<sup>®</sup> approach or a group policy setting. Although not absolutely required, BR&E recommends that Microsoft Visio be installed and functioning prior to installing ProMax.

**During the installation process, ProMax 3.x will uninstall prior versions of ProMax 2.0 or ProMax 1.x that may be installed.** Simultaneous installation of multiple versions of ProMax is not allowed. Earlier 3.x versions of ProMax will not be uninstalled, but rather upgraded to the new release. User customizations made to the Options.xml file will be migrated into the ProMax 3.x files.

You should insure your system meets the minimum software requirements before installing. **ProMax will not run properly on systems that do not meet the minimum software requirements.** Please see the table given earlier that provides the minimum software requirements. BR&E recommends that you keep your system up to date with current service packs and major patches to ensure compatibility now and in the future.

When performing the install, you should select to install the security device driver. In previous versions, the security device driver was required only if a key was physically attached to the system running ProMax. In ProMax 3.x, the driver is required to provide communication with the key in network licensed environments as well. It is recommended that the installation be performed without the security device attached to the system.

If you are using a NetHASP security device, both the NetHASP License Manager (LM) and HASP SRM runtime environment must be installed along with the security key on a system in your network for ProMax to run after installation. You may select any system in your network for this service with a static IP address or hostname resolvable by DNS that is accessible by the workstations that will run ProMax. The NetHASP LM software is present on the DVD in the "HASP & NetHASP" folder. The LM software will also install the driver on the system. Unless the NetHASP LM is accessible via broadcast, the HASP runtime environment will require configuration to specify the address of the system with the network key. This configuration must be made on each system that will run ProMax. In this release, the NetHASP.ini approach has been replaced by a web based console that configures the HASP runtime. The web based application is called the HASP Admin Control Center. The configuration is performed using http protocol on port 1947. To access the configuration section, open your web browser and navigate to the location <http://localhost:1947>. Click Configuration under Administrative Options followed by the Access to Remote License Managers tab. On that page, use the Specify Search Parameters to enter either the IP address or the hostname of the system with the network key. Multiple locations may be specified by placing entries on separate lines. This will be required if separate systems are used to host HASP protected applications from different vendors. Separate host systems are not required with different applications as any number of keys can be attached to a single host. By default, only local administration of the HASP runtime environment is permitted. This can be changed on the Basic Settings tab. For more information concerning the HASP Admin Control Center, select the help links on the appropriate page.

## Performing the Initial Installation of ProMax 3.x from DVD

This procedure is intended for use on systems that do not contain an earlier version of ProMax 3.x, but may contain a version of ProMax 2.x or earlier. If an earlier version of ProMax is installed, you should normally leave it installed so that the settings can be migrated into the current release during installation.

To install the program on these systems, insert the DVD into your system. The system should auto-run the DVD and allow you to start the installation program. If needed, you may start the installation program by running the SETUP.EXE program on the DVD. You should invoke the SETUP.EXE program rather than the MSI file as this program ensures all prerequisite components are installed. The installation program will determine the type of installation that needs to be made (fresh install or upgrade) and perform the appropriate action.

To perform an administrative install, you must run SETUP.EXE with the /a command line option. Note that an administrative install is used for placing ProMax on a file server for distribution using IntelliMirror or other alternative approaches. The administrative install does not actually install the application on the server. Do not confuse an administrative install with the administrator account or elevated privilege requirement for installing on a single workstation.

ProMax requires several prerequisite software packages to be installed before the actual ProMax installation can be attempted. If you install ProMax using the SETUP.EXE program on the DVD, these prerequisite packages will automatically be installed if missing. However, if you install ProMax on workstations in your network using the administrative installation approach or use another alternative installation approach, you must ensure these prerequisites are properly installed before attempting the ProMax installation. Specifically, the Microsoft Core XML Services (MSXML) 6.0 SP1 and Microsoft SQL Server Express 2005 SP3 must be installed prior to installing ProMax. SQL Server Express further requires the Microsoft .Net Framework 2.0 SP2 be installed. For your convenience, these prerequisites are located on the DVD distribution. They are also available from the Microsoft download site, <http://www.microsoft.com/downloads>. SQL Server Express requires special configuration for the ProMax installation to succeed. In particular, a dedicated instance of SQL Express is required. Please see the content of the Prerequisite.xml file for the command line required to install SQL Express. SQL Server Express cannot be installed on systems with less than 512 MB RAM. Under Windows 2000, SQL Server Express will fail to install if MDAC 2.8 SP1 is not installed. When ProMax is removed from the system, the dedicated SQL Server Express instance may also be removed.

If desired, Microsoft SQL Server Express 2008 may be used instead of Microsoft SQL Server Express 2005. Please contact BR&E for instructions on installing Microsoft SQL Server Express 2008.

Depending on the operating system language and version, you may receive an error stating “The Windows Installer service cannot update the system file C:\WINDOWS\system32\msxml6r.dll because the file is protected by Windows. You may need to update your operating system for this program to work correctly.” during the installation of SQL Server Express. This error has been documented by Microsoft in Knowledge Base article 958897 (see

<http://support.microsoft.com/kb/958897>). You may click the OK button to ignore this error as long as no other errors occur during the installation of SQL Server Express. ProMax is distributed with all available languages of SQL Server Express, and this error should not appear unless an English version must be installed on a non-English operating system due to the fact that Microsoft does not supply a version of SQL Server Express for your particular language.

### **Updating Earlier ProMax 3.x Releases using a Windows Installer Patch**

The simplest method to upgrade ProMax is through the FLEXnet Connect service in ProMax. Using this approach, all of the details of downloading and applying the patch are automatically handled. Simply log into an account with elevated installation privileges, and use the FLEXnet Connect Program Manager on the start menu in Windows (labeled Software Updates), or the “Help->ProMax Help->Check for Updates” menu item in ProMax itself to obtain and apply the patch. You may also use the FLEXnet Connect Program Manager to download and save the patch, and subsequently apply it using the instructions below if it is to be applied to multiple systems.

If desired or if you do not use the FLEXnet Connect service, you may download and apply the patch manually. Please contact BR&E if you need the link for the download. The upgrade is distributed as a single compressed Microsoft IExpress executable file containing the patch file (MSP) for the Windows Installer Service. When warranted, BR&E provides two versions of the patch for download. The binary difference patch is a smaller download, but usually requires access to the original ProMax DVD to apply on Windows XP and Windows 2000, but will install on Windows Vista and later without the media. The full-file patch is a larger download, and does not require the original ProMax DVD source. If you extract the MSP patch file from the download executable file, do not attempt to apply the patch by simply double clicking the MSP file in Windows Explorer. You must manually run the Windows Installer program (msiexec) supplying the appropriate command line switches for proper patching to occur. In general, we recommend you apply the patch using the downloaded executable file directly without extracting the MSP file as the proper command line switches are automatically inserted for you. Improper command line switch usage will result in incorrect patching and application failure.

For standalone installations, simply follow these instructions to install the patch (the original DVD distribution may be needed for the binary difference patch as discussed above):

- 1) Log in using an account with elevated privileges.
- 2) Download the patch using the FLEXnet Connect Program Manager or the link supplied by BR&E. If required, supply any required information on the website.
- 3) You may either download and save the patch from the website or run the self-extracting patch file directly without download. If you download the patch, you must run the self-extracting patch file after the download to start the patch process.

To patch a Windows Installer administrative installation used to distribute the application in a network environment, the steps are:

- 1) Download the patch using the FLEXnet Connect Program Manager or the link supplied by BR&E. If required, supply any required information on the website.
- 2) Extract the MSP patch file to a temporary folder from the downloaded patch package.
- 3) Log in using an account with sufficient privileges to modify the administrative share and to force redeployment of the application.
- 4) Patch the administrative share using the command:

```
msiexec /a [Path to Administrative Image]\ProMax.msi /p [Path to MSP Binary Patch]
```

- 5) Force a redeployment of the ProMax application using Active Directory or other approach used to redeploy the application.

### **Upgrading Earlier ProMax 3.x Releases using the DVD Distribution**

The upgrade of earlier ProMax 3.x releases may be accomplished using a ProMax DVD as an alternative to the Windows Installer patch. Since the patch process is typically much faster to perform, the DVD will normally be distributed to customers upon request. To upgrade a standalone installation, simply run the Setup.exe program on the DVD using an account with elevated installation privileges. Do not uninstall the earlier release before performing the upgrade.

If you wish to use the MSI file directly, you must issue the case-sensitive command:

```
msiexec /i [path to DVD]\ProMax.msi REINSTALL=ALL REINSTALLMODE=vomus
```

You cannot simply double click the MSI file in Windows Explorer because the command line options above will not be present. Improper use of command line arguments will result in improper application installation and failure of ProMax to execute properly. The Setup.exe program internally determines the current installation state and starts the msiexec process using the proper command line arguments.

### **Known Issue Upgrading from the ProMax 3.0.9065 Release**

If you receive an error that contains a message with the text `InstallerComponentCodeUpdate` included, please contact BR&E for a workaround. This issue should rarely be encountered.

### **New Features in ProMax 3.2 Relative to ProMax 3.1**

1. Improvements in DGA<sup>®</sup> system predictions have been made through recommendations made by Huntsman Performance Products. For the majority of cases the CO<sub>2</sub> in the treated gas will be lower than in previous versions.
2. User defined physical property packages can now be created as extensibility packages to ProMax. The packages can be written as COM components or as .NET CLR classes using any programming language that supports these technologies.

3. ProMax now supports Microsoft Visio 2010 and the remaining Microsoft Office 2010 products. Microsoft distributes an x64 and x86 version of the Office 2010 products. ProMax is only compatible with the x86 edition, even on x64 operating systems.
4. A new TBP curve library containing almost 200 crudes has been added to the refining examples (file name Crude Oil Library.pmx). The data are stored in an embedded Excel workbook and can be transferred to an oil defined in ProMax. The workbook can be extended to include user defined oils.
5. New tray properties are calculated including jet flood, downcomer flood, and pressure drop for both single and multipass trays. Sieve and round valve trays can now also be specified.
6. The Ionic Info Analysis has been added and calculates compositions of ionic species and the resulting neutral salt species in an aqueous liquid stream. Other properties include Ionic strength, Osmotic Coefficient, p[H] based on concentration, and p[H] based on activity. Consequently, moniker and other associated capabilities are now available for these properties.
7. More options have been added to the Combustion Analysis. The user can select which components to exclude from the analysis. In addition, the stoichiometric oxygen to element (CHSN) ratio can be changed for calculation of the required combustion oxygen.
8. The following heat transfer fluids have been added to the program:
  - Duratherm 450, 600, 630, G, HF, HTO, LT, S, XLT50, XLT120
  - Paratherm CR<sup>®</sup>, GLT<sup>™</sup>, HE<sup>®</sup>, HR<sup>™</sup>, LR<sup>™</sup>, MG<sup>™</sup>, MR<sup>®</sup>, NF<sup>®</sup>
  - Therminol<sup>®</sup> 62, VLT, VP-3
  - Chemtherm<sup>®</sup> 700
  - Chevron: 22, 46
  - UCON<sup>™</sup> 500
  - Mobiltherm<sup>®</sup> 43, 603
  - Coastal HITEC
  - Novo-Ufimsky Oil Refinery, JSC (Novoil) AMT-300
9. The Line Sizing analysis now predicts Erosional Velocity using either the API RP 14E recommended practice or the alternative method proposed by M. Salama. The Line Sizing dialogs have been redesigned for ease of use.
10. The ability to summarize user input data has been added to standard ProMax reports.
11. Two new “wizard” dialogs have been added to the Scenario tool to make it even easier to setup new tests.
12. The phase equilibrium prediction of MTBE containing systems has been improved.
13. Materials of construction for separator sizing and exchanger rating have been updated to the 2010 ASME Boiler and Pressure Vessel Code.

### **New Features in ProMax 3.1 Relative to ProMax 3.0**

1. The Shell Sulfinol process for acid gas treating can be modeled by those companies that have the proper license from Shell. To model Shell Sulfinol, the proper amine mixture must be specified using a component name of “Shell Sulfolane”. The use of “Shell Sulfolane” triggers the use of the properties provided by Shell. Using the generic name “Sulfolane” will not provide the desired properties.

2. Improved the volatility of piperazine in aqueous solutions. Improved the heat of absorption of CO<sub>2</sub> in to aqueous MDEA-piperazine solutions.
3. Added thiosulfuric acid as a dissociating compound with the following reactions:



4. Improved organic sulfur-water systems of DMS-H<sub>2</sub>O, DES-H<sub>2</sub>O, DMDS-H<sub>2</sub>O and CS<sub>2</sub>-H<sub>2</sub>O.
5. Improved predictions of CO<sub>2</sub> and NH<sub>3</sub> in higher concentration CO<sub>2</sub>-NH<sub>3</sub>-H<sub>2</sub>O systems in the presence of urea.
6. Improved O<sub>2</sub> solubility in aqueous amine solutions.
7. Improved HCl-H<sub>2</sub>O vapor-liquid equilibrium predictions.
8. Enhanced salt stencil with thiosulfate salts.
9. A new property has been added to saturators which employ a pure component as the saturant. In previous versions, only the fraction of saturation could be specified. This update allows the mass per standard volume (e.g., lb/MMSCF or g/scm) of the saturant in the outlet stream to be additionally specified.
10. The units for Reid Vapor Pressure (RVP) no longer include the gauge or absolute designator. This is compatible with the reporting of RVP in ASTM D323 along with other publications and government regulations. The change is intended to minimize confusion with the gauge pressure indicator added in ProMax 3.0. While the gauge indicator may no longer be present, the pressure of the apparatus is actually a gauge pressure read from a standard pressure gauge of specified accuracy. No addition of atmospheric pressure is made to the reported reading. Consequently, the magnitude of the value will not change. There are two primary causes of the confusion with RVP units. First, the value is typically reported without the gauge or absolute designation and incorrectly assumed to be an absolute pressure because most vapor pressures are reported in absolute pressure. However, unlike other vapor pressure measurements, the RVP is measured in the presence of approximately one atmosphere partial pressure of air resulting in a gauge pressure that is frequently approximately the same in magnitude as the True Vapor Pressure (TVP) reported in absolute pressure. Second, Note 1 of the ASTM D323 standard states that the RVP is an "absolute" pressure. Unfortunately, this is a poor choice of wording as it does not mean absolute in the sense of absolute versus gauge pressure. Rather, the term means the RVP represents a total pressure.
11. True Vapor Pressures are now expressed in gauge pressure units by default for compliance with various standards including ASTM D1267 and GPA 2140.
12. Adjustments in DEPG (Coastal AGR) system prediction have been made in addition to those previously made in the 3.0 release. Some of the corrections made in the 3.0 release may have overcorrected the results for some applications.
13. The properties of pure argon have been improved.
14. The densities of aqueous glycol solutions have been improved.
15. Heat transfer curve reports for multi-sided heat exchangers now contain a table of heat released or acquired by each exchanger side versus temperature.
16. New multi-sided exchanger shape ("Heat Balancer") allows for connection of multiple single-sided exchangers and separators to form a single unit for reporting and rating.
17. Several new property stencil shapes were added including:
  - a. Pressure/enthalpy isotherm graphing example
  - b. Simple vessel depressurizing calculator

- c. Inline flow multiplier shape
  - d. A shape to transfer heat exchanger internal data to HTRI
18. Enhancements to User Defined reports including:
    - a. Project wide scope facilitating title pages and other single output items
    - b. Improved script handling in pre-process commands
    - c. Ability to define component aliases and groups during reporting
  19. Scenario tool can now manipulate column Murphree efficiencies and also hide Visio to reduce desktop clutter.
  20. Units Set (e.g., SI, US English, etc.) can be selected directly from the menu or toolbar.
  21. The phase envelope analysis will now generate a phase envelope without any user input as the most commonly used parameters are now included as defaults.
  22. Improved the robustness of the NSERC2002 empirical correlations for H<sub>2</sub>, CO, and CS<sub>2</sub> with respect to reactor convergence.
  23. When calculating trayed column flood for low liquid rate service such as glycol contactors, ProMax will no longer issue warnings due to low liquid rate unless the flow parameter is below 0.0001.
  24. The minimum thickness for shells and heads is now set to 1.5 mm in accordance with ASME pressure vessel code part UG-16.
  25. For Separator Sizing and Exchanger Rating, Materials of Construction and formulas for wall thickness or maximum allowable working pressure have been updated to the 2009b Addenda of the 2007 ASME Boiler and Pressure Vessel Code.
  26. For Pipelines and Line Sizing, Thermoplastic Materials of Construction have been updated to The Plastics Pipe Institute TR-4/2009.
  27. For Pipelines and Line Sizing, the OLGAS third-party correlation for multiphase flow has been updated to OLGAS 5.3.2.1. OLGAS is available in ProMax by purchasing a separate license from SPT Group.
  28. The Recycle block now has a "Copy from Inlet" feature to aid in setting an initial guess for the Recycle outlet stream. The user can solve the simulation as an open loop, copy the Recycle inlet stream to the outlet as an initial guess, close the loop, and then allow the Recycle to converge the loop.
  29. Import/Export locations to Excel cells can be moved without the need of deleting and adding.
  30. Addition of an ActiveX control that allows display of property tables in other applications (e.g., Word, Excel, and Visio). This feature can be used to display property tables from different flowsheets together. Property tables can also be combined into a single table.
  31. In Property Tables and Callouts, significant figures can be set for each property individually.
  32. Callout properties can be displayed in vertical as well as horizontal orientation.
  33. Ability to copy/paste from clip board the contents of a Property Table or Callout to other applications such as Excel, Word, etc. Additionally the contents may be pasted directly into the ProMax Visio based flowsheet. Text format carries the full precision on properties. Metafile format (picture) is a snap shot of the control, but can be rotated to any angle if needed. RTF and HTML format can be used for displaying as text but with original precision and symbols.
  34. Thermal efficiencies can now be used in absorbers with side feeds.
  35. Improvements have been made for use of propylene glycol as a heat transfer fluid.

36. The nucleate boiling film correlation can now be selected between the correlations of Mostinski (1963) and Cooper (1984). The Mostinski correlation, which is frequently too conservative, was the only correlation present in previous versions of ProMax.
37. ProMax will utilize some of the capabilities present in the new task bar design of Microsoft Windows 7.
38. For VBA and automation users, more than one instance of ProMax can be created in one application to do side projects.

## **New Features in ProMax 3.0 Relative to ProMax 2.0**

1. The electrolytic models have been extended to characterize more completely the short range ionic interactions that occur in solution. These modifications include the amine-acid gas system and the ammonia-acid gas systems. The changes improve the model predictions for the acid gas vapor-liquid equilibria, and enable better predictions for more concentrated solutions and higher acid gas loadings. For the MDEA-CO<sub>2</sub>-H<sub>2</sub>O system in particular, this has resulted in more optimistic predictions relative to ProMax 2.0 version.
2. The electrolytic models include the dissociation for the following molecular components: Sulfur Dioxide, Phenol, Calcium Hydroxide, and Piperazine.
3. Several improvements have been made with regard to glycol dehydration and glycol injection processes.
  - a. In ProMax 2.0, changes were made based on customer comments that caused the performance of TEG units to be more conservative with respect to water content relative to ProMax 1.2. After release of ProMax 2.0, BR&E decided to scrutinize this problem fully and decided that there were simply insufficient reliable data in critical areas of this process. In some regions, the only data present are graphs that disagree from vendor to vendor, and frequently from publication to publication from the same vendor. Most importantly, these graphs do not provide an indication of how much measured data are used to create them and if true measurements are present in the critical regions. The nature of these data leads to significant design uncertainties, especially for high dew point depression systems. Consequently, BR&E commissioned a study with a reputable research firm with significant experience collecting this type of data to acquire VLE data in these questionable areas. Further, the group was asked to collect data in regions that we felt were known with some confidence to insure the quality of the measurements. The results of this experimental study have been incorporated into ProMax 3.x. Therefore, the user will find that ProMax 3.x will not be as conservative as previous releases of our software and the user should not assume conservative results are generated using ProMax 3.x.
  - b. Improvements in prediction of solubilities of minor components in glycol systems have been made. These include hydrocarbons and various sulfur species. While only small amounts of data are present for many of these minor components, the results from ProMax 3.x should be more reliable than earlier versions.
4. For most systems, ProMax 3.x should require less calculation time than its earlier versions.
5. RVP units have been changed to gauge from absolute pressure. This will require all calculators that use RVP to be adjusted for the new units. Other uses in the program are automatically fixed when the file is read.

6. Projects can now be exported for appending in other projects. A project is exported in its entirety into a file with a pmxexp extension. This file can then be appended to other projects using the File menu. Objects with conflicting names are automatically renamed during the append process. Among other uses, this procedure can be used to create templates of common processes (e.g., dehydration, amine sweetening, refrigeration, etc.) for appending in other projects. Since the process of exporting and appending transfers the project in its entirety, the project upon which the export is based should normally be as simple as possible to prevent deleting unused objects after the append. Please note that you should keep both the standard project file (pmx) along with the export file (pmxexp). The export file is specific to the version of Visio used to create it and will need to be recreated from the pmx file when a Visio upgrade is made.
7. Improvements in predictions for DEPG (Coastal AGR) systems have been made. Among the many improvements include better prediction of high hydrogen systems such as those involved in synthesis gas treating. Improvements in hydrocarbon solubility predictions have also been made.
8. The ability to model gas treating (including synthesis gas) using the physical solvent propylene carbonate has been added. The recommended property package for this system is either Peng-Robinson or SRK.
9. Extractive processes for olefins and acetylenes utilizing N,N-Dimethylformamide (DMF) can now be modeled. The appropriate property packages include either the Gibbs excess models (e.g., NRTL) or Peng-Robinson Polar or SRK Polar.
10. Pertinent information from GPA Standard 2145-09 has been added to ProMax due to its recent adoption.
11. The correlations in Figure 22-10 of the 12<sup>th</sup> edition GPSA Engineering Databook for COS and CS<sub>2</sub> hydrolysis have been added. These correlations can be added to any Claus bed to model the hydrolysis of COS and CS<sub>2</sub> into H<sub>2</sub>S and CO<sub>2</sub>. The correlations are for activated alumina catalysts. Other catalysts will yield different performance. In addition, a new Gibbs set named "GPSA Hydrolyzing Claus Bed" has been created that will automatically add these correlations to a Gibbs minimization reactor. The previous "Hydrolyzing Claus Bed" has been renamed to "Equilibrium Hydrolyzing Claus Bed" to indicate that the hydrolysis is modeled at equilibrium. While normally predicting a conversion less than equilibrium conversion, the GPSA hydrolysis correlations can predict a conversion that exceeds equilibrium conversion at certain conditions. This fact is a general statement for any conversion correlation. When this occurs, a warning is provided in the reactor. One remedy for this warning is to deactivate the constraint of the offending component (usually COS) so that it is modeled at equilibrium. The component must remain active in the reactant list or it will be considered an inert. Alternatively, a linear constraint may be constructed to limit the conversion.
12. The following changes have been made to the heat exchanger rating program:
  - a. Double pipe heat exchangers can now rate Inline (straight path) as well as Hairpin (U-tube) type exchangers.
  - b. Heat transfer film coefficients have been improved, especially for boiling and condensation conditions. Calculation of condensation film coefficients has been made less aggressive when non-condensables are present.
  - c. Several issues affecting calculations of tube count and total area have been resolved.
  - d. Several issues in heat exchanger pressure drop calculations have been resolved.

- e. Impingement calculations and recommendations for shell and tube exchangers have been improved.
  - f. The ProMax double pipe shell side interface has been simplified to remove unnecessary properties.
  - g. Several new properties have been added and are described in the ProMax Help. Specific properties at each side increment are grouped on a Detail tab apart from the more general properties.
13. The cross exchanger properties Minimum End Approach Temperature, Log Mean Temperature Difference and End Point UA can now be set by the user. A direct solution will only be obtainable for those cases in which at least two of the connected streams can be solved independently *before* the cross exchanger is called upon to solve for the remaining streams. Other cases will require a recycle with initial guess for calculation.
  14. Tooltips that display values in common units are shown when the mouse is placed over a value. These tooltips can be disabled by the user if desired. Further, the units which are displayed for a value can be configured by modification of the Options.xml file.
  15. Reporting flexibility has been greatly increased with the user capability to define templates for Microsoft® Excel reporting. These templates are standard Excel workbooks that are edited with a report editor supplied in the Excel Add-In “ProMax User Defined Report.xla” located in “%ProgramFiles%\Bryan Research & Engineering\ProMax3\AddOns\Excel” folder. The editor gives the ability to place ProMax data in locations while leaving other aspects of formatting and layout to the familiar tools built into Excel. Report templates can be applied to any ProMax project via ProMax’s Report dialog. For further information or assistance with template creation, please contact our technical support group at [support@bre.com](mailto:support@bre.com).
  16. A custom property package is no longer required to obtain liquid densities from the equation of state. When applicable, the density selection in the environment will allow the EOS density to be selected in addition to either COSTALD or Rackett. EOS densities normally provide better estimates for the liquid in the critical region. The application of EOS densities will most commonly be encountered in CO<sub>2</sub> acid gas injection systems.
  17. The Span and Wagner equation of state for pure CO<sub>2</sub> was implemented based on Span, R., Wagner, W., *J. Phys. Chem. Ref. Data*, Vol. 25, No. 6, 1996, pp. 1509-1596. This equation of state represents most experimental data within experimental uncertainties. It produces exceptional accuracy in the critical region. In addition, in technically important regions up to pressures of 30MPa and up to temperatures of 523K, the estimated uncertainty of the formulation ranges from ±0.03% to ±0.05% in density and ±0.15% to ±1.5% in the isobaric heat capacity. This empirical formulation is valid in the fluid region up to temperatures of 1100K and at pressures up to 800 MPa. This model can be used to model acid gas injection systems without water present to determine if the properties computed by other EOS's such as Peng-Robinson or SRK are accurate enough for use. Since this equation of state is a pure fluid equation of state, no hydrate predictions can be made with this package.
  18. The IAPWS (International Association for the Properties of Water and Steam) Formulation 2001 for Thermodynamic Properties of Ammonia-Water mixtures presented in *Guideline on the IAPWS Formulation 2001 for the Thermodynamic Properties of Ammonia-Water Mixtures*, The International Association for the Properties of Water and Steam, Gaithersburg, Maryland, 2001, has been added as the Tillner-Roth and Friend NH<sub>3</sub> + H<sub>2</sub>O Property Package. This correlation provides the most accurate description of thermodynamic

properties of ammonia-water mixtures available at the time it was developed over a wide range of conditions. It is valid in the vapor and liquid phases for pressures up to 40 MPa. The formulation represents the vapor-liquid equilibrium properties with an uncertainty of  $\pm 0.01$  in liquid and vapor mole fractions. In the single phase region, uncertainties are estimated from  $\pm 0.3\%$  to  $\pm 1\%$  in vapor density and from  $\pm 0.3\%$  to  $\pm 2\%$  in liquid density, and  $\pm 200$  J/mol for enthalpies. This model can be used to represent ammonia-water mixtures as the working fluid in absorption refrigeration cycles or other systems where binary ammonia-water mixtures are encountered. Additionally, the equation of state for pure ammonia presented by Tillner-Roth, R., Harms-Watzenberg, F., Baehr, H.D., *Eine neue Fundamentalgleichung für Ammoniak*, Proc. 20<sup>th</sup> DKV-Tagung Heidelberg, Germany, Vol. II, 1993, pp. 167-181, has been added. The ammonia correlation provides a good description of the thermodynamic properties of ammonia over a wide range of measurements available at the time this correlation was formulated. Finally, the IAPWS Formulation 1995 for Thermodynamic Properties of Water implemented by Wagner, W., Pruss, A., *J. Phys. Chem. Ref. Data*, Vol. 31, No. 2, 2002, was added. This formulation covers a range of temperatures from the melting line (lowest temperature 251.2K at 209.9 MPa) to 1273K and pressures up to 1000 MPa. In the liquid region, the estimated uncertainty ranges from  $\pm 0.001\%$  to  $\pm 0.02\%$  in density and  $\pm 0.1\%$  in the isobaric heat capacity. In the gas region, the estimated uncertainty ranges from  $\pm 0.03\%$  to  $\pm 0.05\%$  and  $\pm 0.2\%$  in the isobaric heat capacity. In the critical region, the IAPWS-95 formulation represents with a very good accuracy both thermal and caloric properties.

19. The individual diatomic deuterium ( $D_2$ ) modifications are now present in ProMax. The program includes orthodeuterium, paradeuterium, equilibrium deuterium, and normal deuterium. The previous versions of the program only included normal deuterium. Normal deuterium is a constant composition mixture of 75% paradeuterium and 25% orthodeuterium. ProMax will accurately predict the equilibrium distribution of para and ortho deuterium in a Gibbs free energy minimization reactor. If the generic names for diatomic deuterium (i.e.,  $D_2$ , Deuterium) are selected as components, the program will use normal deuterium as in the past.
20. Materials of Construction for pressure vessels and exchanger rating have been updated to the 2007 ASME Boiler and Pressure Vessel Code, including the 2008a Addenda.
21. Thermoplastic piping is now available as a Material of Construction in the Pipeline block and Line Sizing analysis.
22. In the Line Sizing analysis, two additional pressure design codes are available for calculating the Maximum Allowable Working Pressure:
  - Canadian Standards Association CSA Z662 *Oil and Gas Pipeline Systems*
  - ASME B31.4 *Pipeline Transportation Systems for Liquid Hydrocarbons and Other Liquids*.
23. The materials in CSA Z245.1 "Steel Pipe" are available as Materials of Construction for Line Sizing and Pipelines.
24. In the Line Sizing analysis, the B31.3 pressure code has been updated to include the Weld Joint Strength Reduction Factor, which was added to the design equation by errata in ASME B31.3-2006. The coefficient Y has also been added. Both of these parameters are calculated by ProMax or can be optionally specified by the user.
25. Standard Dimension Ratio (SDR) pipe sizes and all pipe sizes from ASME B36.10M are now available in the Line Sizing analysis and the Pipeline. Pipe sizes can be specified in either

Nominal Pipe Size (NPS) or Diameter Nominal (DN), which is the dimensionless designator used in the metric system to describe pipe size. The NPS, DN, and thickness can be selected from dropdown lists of the sizes available for the specified Pipe Schedule.

26. Absolute Roughness values for common pipe materials can be selected from dropdown lists in Pipelines and Line Sizing analyses.
27. Pipeline enhancements include:
  - The Initial Value Method, either EPISODE or Runge-Kutta, can now be selected when the Continuous Solution Method is specified. EPISODE is the default, but Runge-Kutta may solve faster in some cases.
  - An option to Check Freezeout per Increment has been added. By default, it is unchecked, and Freeze Out will be checked only at the beginning and end of the pipeline and between segments or fittings. If this property is check-marked, then Freeze Out will be checked at every increment to determine exactly where freeze out begins or is within range of freezing.
  - For pipelines with multiple pipe segments, if only one Ambient Temperature is specified, all other segments will default to this Ambient Temperature. For wells with specified elevation changes in the segments, if at least two Ambient Temperatures are specified, the other Ambient Temperatures will be calculated based on the elevation gradient of the specified temperatures.
  - Pressure drop through valves and fittings can now be calculated using the Equivalent Length ratio, L/D, which may be more accurate than the Fitting Kv calculation for compressible flow, especially near sonic velocity.
28. Distillation Column Hardware properties can now be specified directly in the Hardware dialogs. The Edit dialogs have been removed.
29. ProMax can now be used to size liquid-liquid columns by using the liquid load (total liquid flux) on a stage. Specify either the diameter or the liquid load (which is sum of both liquid flows on stage) and the other parameter is calculated. For amine liquid-liquid columns, recommended liquid loads are 15 gpm/ft<sup>2</sup> (610 lpm/m<sup>2</sup>) for gas plants and 10 gpm/ft<sup>2</sup> (405 lpm/m<sup>2</sup>) for refinery service.
30. Distillation columns now allow Murphree Efficiencies greater than 100%, which can be useful to fine tune predictions to operating data for amine and other columns.
31. The dialogs for the Recycle/Propagation Terminal have been redesigned for ease of use.
32. The advanced solver and specifier provide additional flexibility in the calculation source. Previously only Excel and VBScript or JScript were allowed. In the current version, the option of using Visual Basic for Applications (VBA) in Visio or Excel and the use of an external COM object written in any COM compliant programming language are available. ProMax can directly call the COM object, or you can connect your implementation to ProMax using COM connection points (events). The connection point method is also available in VBA. These new capabilities make it easier to create solvers and specifiers based on programs that may already be internally available.
33. The combustion analysis will now calculate heating values on a molar, mass, and volumetric basis. In addition, the combustion and metering temperatures may be specified at the combustion analysis level to serve as the basis for computation. For more information, see GPA Standard 2172 and ISO 6976.

34. ProMax Property Stencil has been expanded with several new calculation shapes, a simple membrane and orifice plate block. Two selection shapes were also included to assist users in creating their own block shapes, and to add default values and calculators to block shapes.
35. The *Bottoms Head* specification has been added to the staged column properties to account for the liquid head between the bottom of the column and the reboiler.
36. Sizing a three phase separator no longer requires a vapor flow.
37. Petro-Therm™ and Shell Thermia® C heat transfer fluids have been added.
38. The units TR for ton of refrigeration and RT for refrigeration ton have been added.
39. Adjustments and bug fixes have been made to curve oils. If the user wishes to incorporate these changes into existing flowsheets the oil must be recharacterized manually by the user. This can be done by modifying something in the characterization.
  - The easiest way to recharacterize the boiling point data is by changing the Assay Type and then resetting to the original Assay Type.
  - The easiest way to recharacterize user supplied curve data for specific gravity and molecular weight is to edit the data, alter the amount for the highest or lowest fraction distilled, click OK, and then reedit the data restoring the original value.
  - The easiest way to recharacterize user supplied curve data for high and low temperature viscosity is to delete the Viscosity Assay temperature and hit enter to restore the temperature.
40. Most examples have been updated and several new examples have been added to demonstrate new or improved features of the program.
  - An MDEA Sweetening with Piperazine example has been added to the Amine Sweetening folder.
  - A pair of examples has been added to the Calculators folder to demonstrate new calculator Source Types, a VBA type and an Event Based type (using VBA).
  - The Gas Processing folder contains new JT examples, a GSP unit, and a propylene carbonate unit for synthesis gas treatment.
  - The Refining folder contains many new examples: Benzene Removal from Fuel Stock, Butadiene Extraction using DMF, Hydrogen Production and Purification, a new Coker Fractionation column with side strippers, an FCC Fractionation column, and an FCC SO<sub>2</sub> Offgas Scrubber.
  - Most Sulfur Recovery examples have been converted to employ the GPSA Hydrolyzing Claus Bed Gibbs Set.
  - A new Power and Refrigeration folder demonstrates the setup of ammonia absorption refrigeration, Kalina and Rankine cycles, and refrigerant systems.The examples have been solved in ProMax 3.x and each example is ready for inspection
41. Several bug fixes have been made.

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